

27 febbraio 2019  
Incontro del  
Gruppo di lavoro sui  
BIOFILM

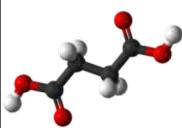
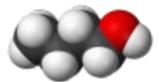
Società dei Naturalisti in  
Napoli, via mezzocannone 8  
Ore 9.30

**UNIVERSITA' degli Studi di Napoli Federico II**  
Dipartimento di Ingegneria Chimica dei Materiali  
e della Produzione Industriale  
(DICMaPI)/  
**Istituto di Ricerche sulla Combustione (IRC) - CNR**  
gruppo di lavoro  
Componenti:

- Antonio Marzocchella (DICMaPI)
- Piero Salatino (DICMaPI)
- Francesca Raganati (DICMaPI)
- Maria Elena Russo (IRC-CNR)

# Tematiche di interesse

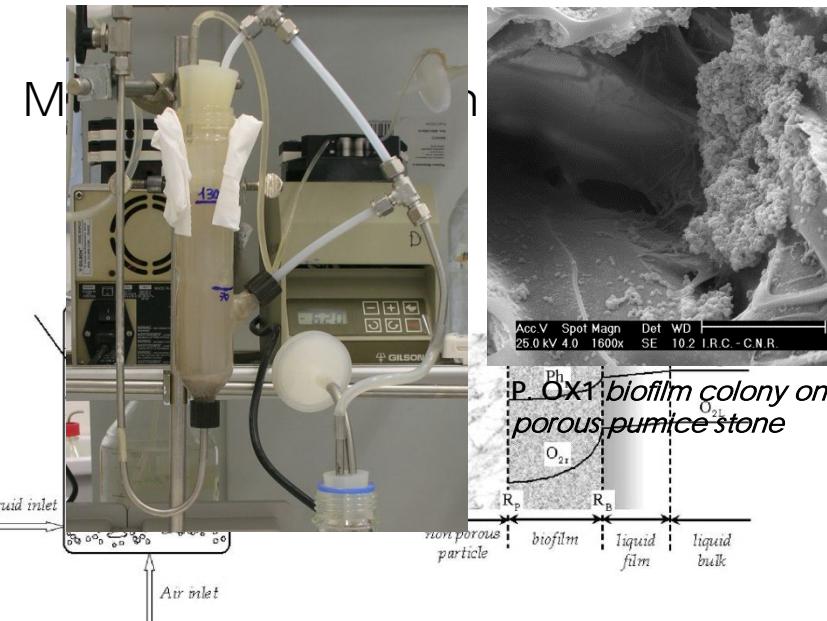
- Previous activities on **biofilm reactors**
  - *Phenol degradation by Pseudomonas OX1 biofilms*
  - *Butanol production by Clostridium acetobutylicum biofilms*
- **Biobutanol** production in a series of 4 biofilm reactors
- **Succinic acid** production
  - *Packed bed biofilm reactor (PBBR)*
  - *Fluidized bed biofilm reactor (FBBR)*



2004

# Aerobic biofilm reactors: phenol degradation by *Pseudomonas stutzeri*

Lab scale biofilm reactors: degradation of phenol and azo-dyes by *Pseudomonas OX1* biofilm on porous granular supports



2011

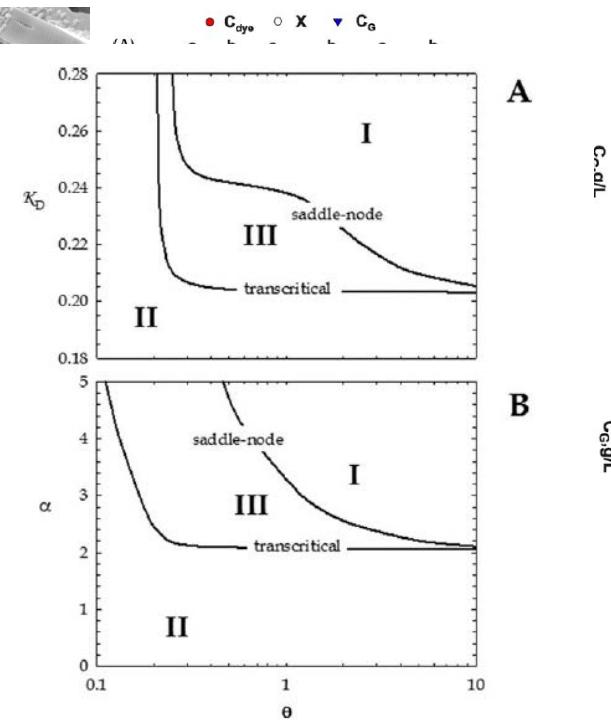
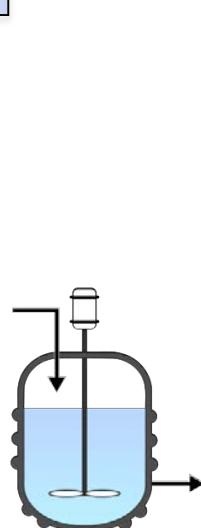
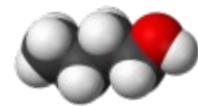


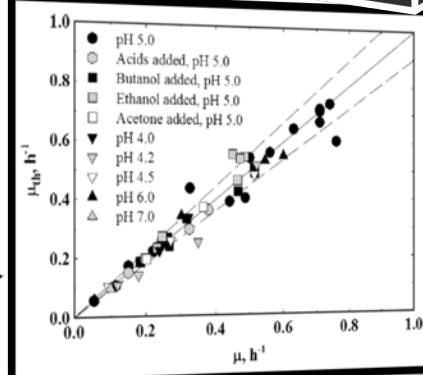
Figure 6. Bifurcation maps: (A)  $\theta$  vs.  $K_D$  ( $\alpha = 2$ ,  $K_L = 200$ ); (B)  $\theta$  vs.  $\alpha$  ( $K_D = 0.2$ ,  $K_L = 200$ ). Roman numerals indicate the number of steady-state solutions.

2006

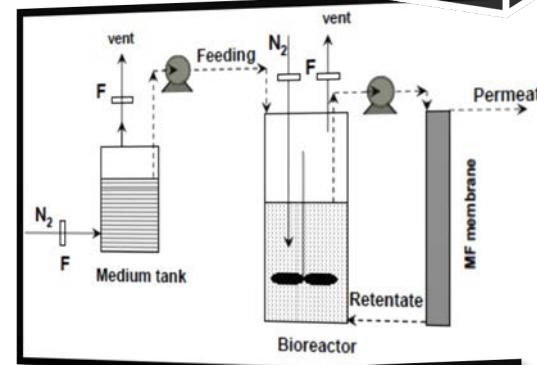
# ACETONE – BUTANOL – ETHANOL production by *Clostridium acetobutylicum*



## Acidogenesis Kinetics



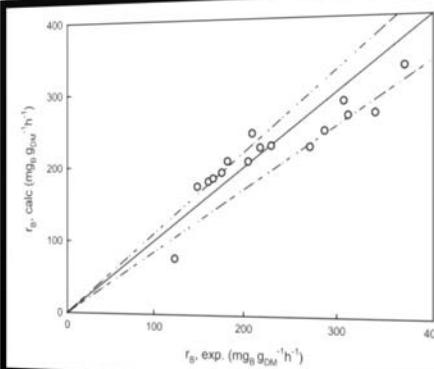
## Solventogenesis Kinetics



$$\mu = \mu_{max} \cdot \frac{L}{L + K_L} \cdot \left(1 - \frac{AA}{AA_{max}}\right)^{n_{AA}} \cdot \left(1 - \frac{BA}{BA_{max}}\right)^{n_{BA}} \\ \cdot \left(1 - \frac{Ac}{Ac_{max}}\right)^{n_{Ac}} \cdot \left(1 - \frac{Et}{Et_{max}}\right)^{n_{Et}} \cdot \left(1 - \frac{B}{B_{max}}\right)^{n_B}$$

$$\mu_{max} = 0.95 \text{ h}^{-1} \quad K_L = 1.34 \text{ g/L} \\ AA_{max} = 1.56 \text{ g/L} \quad n_{AA} = 0.98 \\ BA_{max} = 3.00 \text{ g/L} \quad n_{BA} = 0.96$$

$$Ac_{max} = 64.5 \text{ g/L} \text{ and } Et_{max} = 35.0 \text{ g/L}$$



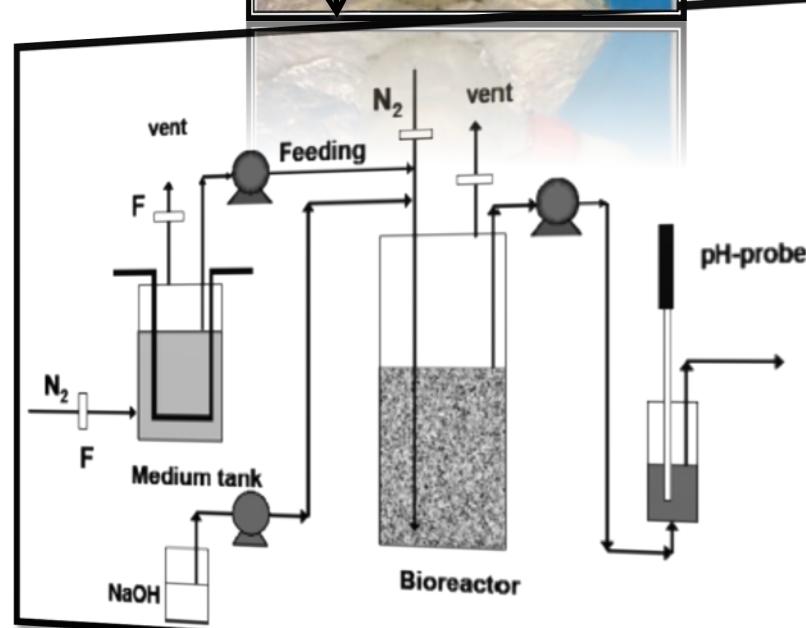
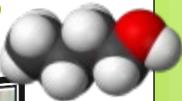
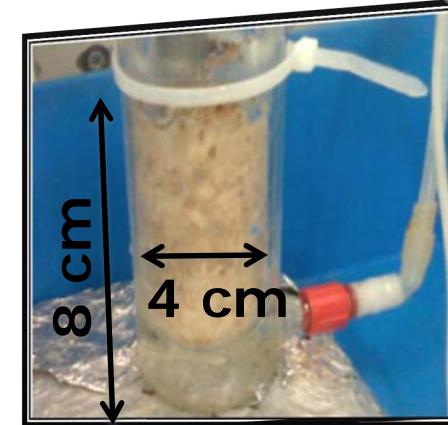
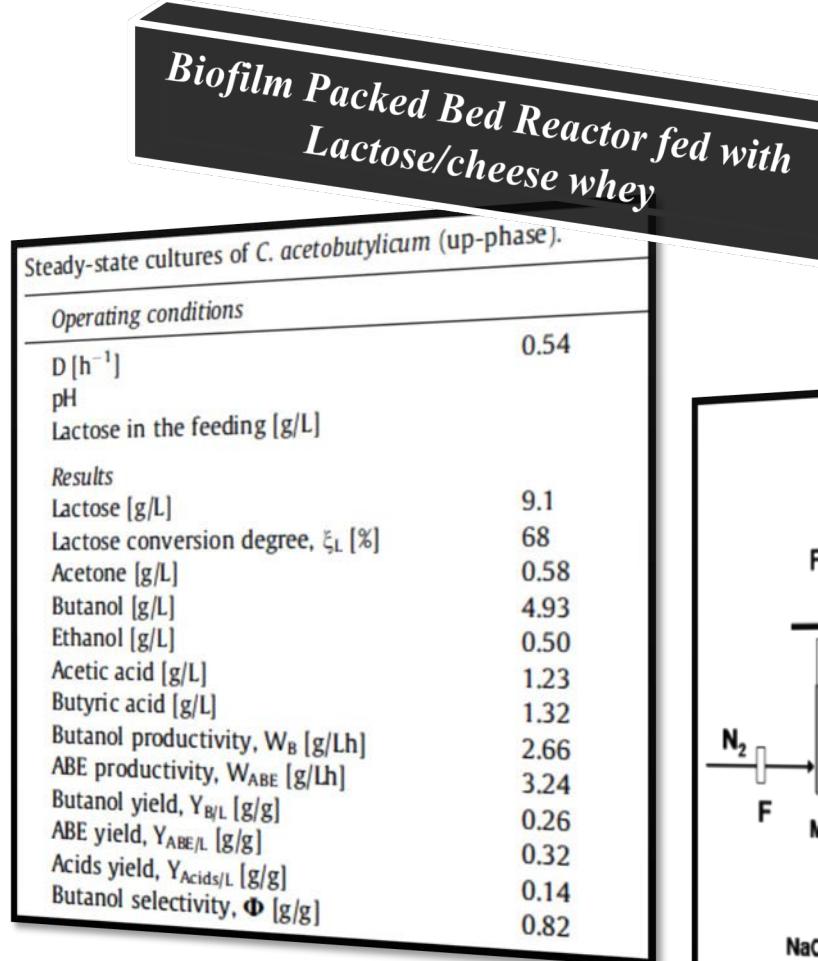
$$r_B = r_{B,max} \left( \frac{C_L}{K_{LB} + C_L} \right) \left( \frac{AA}{K_{AA} + AA} \right) \left( \frac{BA}{K_{BA} + BA} \right) \left( \frac{K_B}{K_B + B} \right)$$

[5] Napoli et al. (2012). Enzyme and Microbial Technology. 50:165-172.

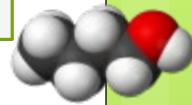
[6] Napoli et al. (2011). Bioresource Technology. 102:1608-1614.

# ABE production by *Clostridium acetobutylicum*

2010

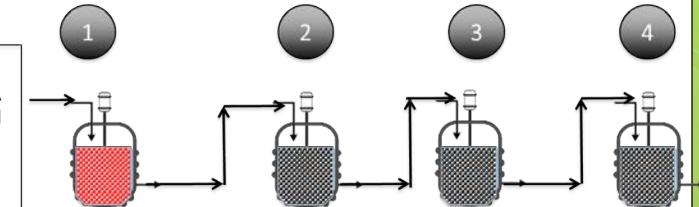
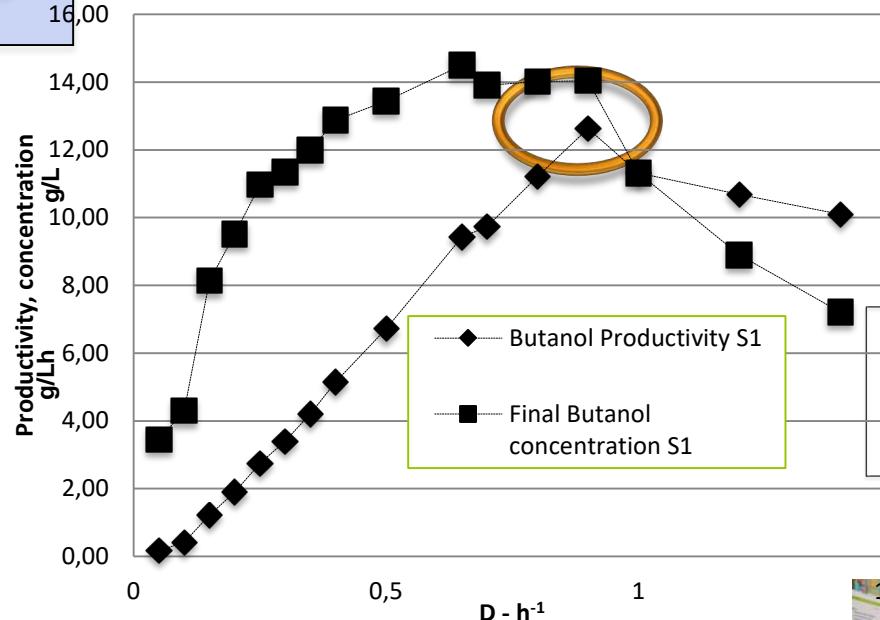


2012



# ABE production in a series of 4 biofilm reactors

2013



WASTE2FUELS

Sustainable production of next generation  
biofuels from waste streams-

Grant Agreement 654623 H2020 – LCE-11-2015

2018

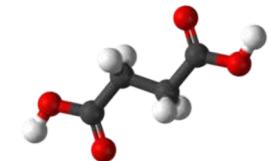


[8] Raganati et al., patent RM2015A000185 (2015)

[9] Raganati et al. (2016). Chem Eng Sci. 152: 678-688.

2015

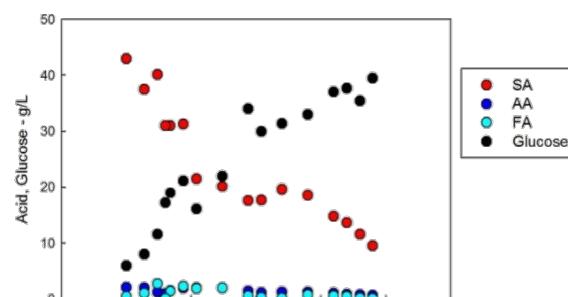
# SUCCINIC ACID PRODUCTION by *Actinobacillus succinogenes*



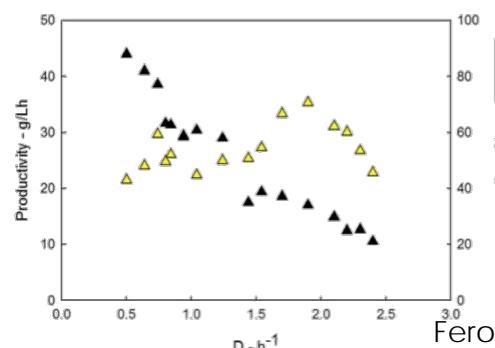
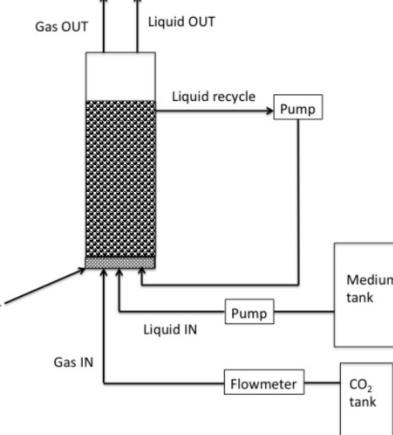
*Growth Kinetics*

*Characterization of the Conversion Process*

*Packed bed biofilm reactor (PBBR)*



*Fluidized bed biofilm reactor (FBBR)*



Ferone et al. (2018). Biotechnol. Biofuels 1–11.

Ferone et al. (2018). Appl. Biochem. Biotechnol. <https://doi.org/10.1007/s12010-018-2846-8>

Ferone et al., (2017). Appl. Biochem. Biotechnol. doi:10.1007/s12010-017-2514-4

2018

# Prospettive future

- **Syngas fermentation** for the production of bio-fuels (butanol) and bio-commodities (bio-polymers)
- Application of BIOFILM REACTORS to bioconversion processes: sharing expertise in modelling, design, lab-scale set up and operation for interdisciplinary projects.

# Prospettive future

**Naples Summer school:**  
‘Biofilm fundamentals and application’??

Summer 2020??

Lecture sessions??  
Practice sessions??